B & L Cremations Systems, Inc.

February 16, 2011 Page 1

Planning and Zoning Commission

Project: Proposal Human Crematory

To Whom It May Concern:

This letter will provide certain facts and information regarding the placement of our UL listed class 6 type IV human cremation equipment within residential, commercial or industrial zoned areas.

The primary purpose of this information is to provide background on our company, detailing our experience, in the cremation equipment market to you and any others that might review this document. Also, enclosed is factual information regarding the general location and operating conditions of cremation equipment throughout the United States.

B & L Cremation Systems has been designing, engineering, manufacturing and installing combustion systems for a wide range of industries for over 25 years. We are recognized as the leader in cremation equipment design and engineering, and are the world's largest independent manufacturer of cremation equipment. With nearly 2,000 installations throughout the United States and over 50 countries, our designs have been granted U.S. patents, and have been adopted as industry standards for quality and performance. In addition, we are one of the largest service and repair organizations, servicing all brands of cremation equipment.

Our equipment operates without smoke or odor, almost every installation must be permitted by the environmental authorities for the city, state or province in which it is installed. The equipment we manufacture is Underwriters Laboratories (UL) listed, confirming maximum safety of both equipment and personnel.

Each model manufactured by our company has been personally designed and engineered by Dr. Steve Looker and tested by an independent testing laboratory against standards set forth by the federal government. Our equipment's emission levels are less than half the allowable standards to ensure environmental quality. Residents of the area may not be aware that the equipment is operating.

All equipment that performs combustion, from automobiles or furnaces of any type (fireplaces or crematories), give off byproducts of which some are referred to as particulate matter. Because of our equipments high quality standards, these byproducts are not visible, nor is there an odor from the material being combusted. The equipment operates automatically and has built-in pollution detection equipment that constantly supervises the operation, safeguarding against pollution and environmental impact.

Noise levels are not detectable from outside the building and are therefore insignificant. Cycle time is dependent on size of load. When this cycle time is multiplied by the annual frequency of use, the actual hours of operation can become insignificant.

Planning and Zoning Commission February 2011 Page 2

I have enclosed a chart comparing combustion by an automobile, a diesel truck, and a cremator operating a two-hour period (the cycle time of a cremation). As you can clearly see, the cremator has far lower emission levels. The data on the automobile and truck comes from the United States governments AP42 emission levels document, and the information regarding pollutants from the crematory is based on actual test results.

I appreciate your interest and concern regarding the basic information surrounding the installation of cremation equipment. Please feel free to distribute this letter of information to any individuals and/or groups that might have interest.

Should you or others require additional information or have questions about anything in this letter, please call me using our toll-free number 800-622-5411 ext: 103.

Sincerely,

Dr. Steve Looker Phd Environmental Engineer

EMISSIONS TESTING of the FIRST CALL CREMATORY B & L CREMATION SYSTEMS, INC. N20 SERIES HUMAN CREMATORY Clearwater, Florida

April 5, 2008

FDEP Permit No. 1030473-008AG EU No. 008 SES Reference No. 08S131

Conducted by:

SOUTHERN ENVIRONMENTAL SCIENCES, INC. 1204 North Wheeler Street Plant City, Florida 33566 Phone (831) 752-5014, Fax (813)752-2475

Project Participants

Byron E. Nelson Mark S. Gierke Dale A. Wingler Travis B. Nelson

SPECIAL EMISSIONS

EMISSION TESTING

of the

FIRST CALL CREMATORY B & L CREMATION SYSTEMS, INC. N20 SERIES HUMAN CREMATORY

Clearwater, Florida

April 5, 2008

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1.0 INTRODUCTION

Southern Environmental Sciences, Inc. conducted emissions testing of the First Call Crematory, B & L Cremation Systems, Inc. N20 Series human crematory on April 5, 2008. This facility is located at 12660 34th Street North, Clearwater, Florida. Testing was conducted for particulates, carbon monoxide (CO), sulfur dioxide (SO₂), nitrogen oxides (NOx), total hydrocarbons (VOC) and visible emissions. Oxygen (O₂) concentrations were measured to correct emission rates to 7% O₂. Mr. Jose Rodriguez of the Pinellas County Department of Environmental Management was present as an observer during a portion of the testing.

2.0 SUMMARY OF RESULTS

Results of the particulate, carbon monoxide, sulfur dioxide, nitrogen oxides and total hydrocarbons are summarized in Table 1. A visible emissions evaluation was performed over a one hour period. The average maximum six minute opacity was zero percent.

3.0 PROCESS DESCRIPTION

The B & L Cremation Systems N20 Series crematory incinerator cremates human remains in an environmentally acceptable manner. The unit consists of a primary and secondary (afterburner) chamber each fired with natural gas. The unit is designed to incinerate human remains at a rate of 150 pounds per hour with a maximum heat input rate of 1.5 MMBTU per hour (primary chamber 0.5 MMBTU per hour, secondary chamber 1.0 MMBTU per hour).

TABLE 1. EMISSIONS TEST SUMMARY

Company: FIRST CALL CREMATORY

Source: B & L Cremation Systems, Inc.

N20 Series Human Crematory

	Run 1	Run 2	Run 3
Date of Run	4/5/08	4/5/08	4/5/08
Weight of Human Remains (lbs.)	170	165	140
Start Time (24-hr. clock)	1005	1348	1722
End Time (24-hr. clock)	1107	1452	1824
Vol. Dry Gas Sampled Meter Cond. (DCF)	39.324	47.848	41.832
Gas Meter Calibration Factor	0.994	0.994	0.994
Barometric Pressure at Barom. (in. Hg.)	30.39	30.29	30.39
Elev. Diff. Manom. To Barom. (ft.)	, 0 .	0	0
Vol. Liquid Collected Std. Cond. (SCF)	3.305	5.073	2.966
Moisture in Stack Gas (% Vol.)	7.8	9.9	8.6
Molecular Weight Wet Stack Gas	28.48	28.17	28.62
Stack Gas Static Press. (in. H2O gauge)	-0.03	-0.03	-0.03
Average Square Root Velocity Head	0.166	0.208	0.187
Average Orifice Differential (in. H2O)	1.132	1.669	1.291
Average Gas Meter Temperature (°F)	81.5	88.3	91.7
Average Stack Gas Temperature (°F)	834.3	1013.6	998.3°
Pilot Tube Coefficient	0.84	0.84	0.84
Stack Gas Vel. Stack Cond. (ft./sec.)	16.78	19.88	17.65
Effective Stack Area (sq. ft.)	1.87	1.87	1.87
Stack Gas Flow Rate Std. Cond. (DSCFM)	623	715	659
Stack Gas Flow Rate Stack Cond. (ACFM)	1,833	2,202	1,977
Net Time of Run (min.)	60	60	6 0
Nozzle Diameter (in.)	0.600	0.600	0.600
Percent Isokinetic	98.7	102.6	97.6

TABLE 1. EMISSIONS TEST SUMMARY (con't)

Company: FIRST CALL CREMATORY

Source: B&L Cremation Systems, Inc.

N20 Series Human Crematory

	Run 1	Run 2	Run 3	
Date of Run	4/5/08	4/5/08	4/5/08	
Weight of Human Remains (lbs.)	170	165	140	
Start Time (24 hr. clock)	1005	1348	1722	
End Time (24 hr. clock)	1107	1452	1824	
Oxygen (%)	12.7	12.1	13.1	
Particulate Collected (mg.)	27.0	69.1	99.2	
,				
•				(Avg.)
Particulate Emissions (gr./DSCF)	0.011	0.023	0.038	0.024
Particulate Emissions (gr./DSCF @ 7% O2)	0.018	0.036	0.066	0.040
Particulate Emissions (lb./hr.)	0.06	0.14	0.21	0.136
CO Emissions (ppm)	3.05	2.27	4.98	3.43
CO Emissions (ppm @ 7% O2)	3.4	2.95	6.7	4.35
CO Emissions (lb./hr.)	0.007	0.006	0.018	0.010
370 F 5 1 4 4	110.00	100.0	1157	1161
NOx Emissions (ppm)	110.23	122.3	115.7	116.1
NOx Emissions (lb./hr.)	0.58	0.71	0.74	0.677
VOC Emissions (ppm)	1.5	0.80	1.41	1.237
VOC Emissions (lb./hr.)	0.007	0.004	0.009	0.007
VOC Emissions (10.7m.)	0.007	0.004	0.009	0.007
SO ₂ Collected (mg)	33.1	49.4	59.7	47.4
SO ₂ Emissions (lb./hr.)	0.088	0.142	0.167	0.13
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Note: Standard conditions 68°F, 29.92 in. Hg

1.0 MMBTU/hr.). Emissions are controlled by the afterburner that is preheated and maintained at a minimum operating temperature of 1600°F prior to and during ignition of the primary chamber. Process operational data was provided by facility personnel and is included in the appendix.

4.0 SAMPLING PROCEDURES

4.1 Methods

All sampling was performed using methods currently acceptable to the FDEP. All test methods are contained in Title 40 of the Code of Federal Regulations, Appendix A and are as follows:

Pollutant	EPA Method No.	Title
Particulates	5	Determination of Particulate Emissions from Stationary Sources
Carbon Monoxide	10	Determination of Carbon Monoxide Emissions from Stationary Sources
Oxygen	3B	Gas analysis for the Determination of Emissions Rate Correction Factor or Excess Air
Nitrogen Oxides	7E	Determination of Nitrogen Oxides Emissions from Stationary Sources (Instrumental Analyzer Procedure)
Sulfur Dioxide	6	Determination of Sulfur Dioxide Emissions from Stationary Sources, Section 2.1
Total Hydrocarbons	25A	Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer
Visible Emissions	9	Visual Determination of the Opacity of Emissions of Stationary Sources.

Sulfur dioxide emissions were determined simultaneous with particulates as per Section 6.1 of EPA Method 6.

4.2 Sampling Locations

Locations of the sample ports and stack dimensions are shown in Figure 1.

Particuale/SO₂ sampling was accomplished by conducting horizontal traverses through each of two ports located on the stack at a ninety degree angle from one another. Twenty four sample points were chosen in accordance with EPA Method 1 – Sample and Velocity Traverses for Stationary Sources, 40 CFR 60, Appendix A. Carbon monoxide, nitrogen exides, total hydrocarbon and exygen sampling were performed from the same sampling ports as the particulate/SO₂ sampling.

4.3 Sampling Trains

The particulate/SO2 sampling train consisted of a 3 foot Inconnel probe utilizing a one piece quartz glass nozzle and liner, a heated glass fiber filter and four impinges arranged as shown in Figure 2. Flexible tubing was used between the heated filter and the impingers. The first impinger was charged with 100 milliliters of 80% isopropanol, the second and third impingers were each charged with 100 milliliters of a 3% percent hydrogen peroxide solution and the fourth impinger was charged with indicating silica gel desiccant. The impingers were cooled in an ice and water bath during sampling. A Nutech Corporation control console was used to monitor the gas flow rates and stack conditions during sampling.

The carbon monoxide sampling train consisted of a stainless steel probe, Teflon sample line, condenser, silica gel and carbon dioxide adsorbent tubes and a Thermo Environmental Instruments, Inc. Model 48 Gas Filter Correlation CO analyzer arranged as shown in Figure 3.

The nitrogen oxides sampling train consisted of a stainless steel probe, Teflon sample line, and a California Analytical Inc. Model 300 FID analyzer arranged as shown in Figure 5.

The oxygen sampling train consisted of a probe, sample line, tedlar bag in a rigid container, valve, vacuum pump, and flow meter.

4.4 Sample Collection

Prior to particulate/SO₂ sampling, the pitot tubes were checked for leaks and the manometers were zeroed. A pretest leak check of the sampling train was conducted by sealing the nozzle and applying a 15" Hg vacuum. A leak rate of less than 0.02 cubic feet per minute was considered acceptable. Sample was collected isokinetically for two and one half minutes at each of the points sampled.

All instrumental analyzers were calibrated immediately prior to the beginning and checked after each run by introducing known gases into the instrument through the sampling.

The tedlar bag used for obtaining an integrated oxygen sample was leak checked prior to the test by pressurizing it to 2 to 4 in. H₂O and allowing it to stand overnight. The bag was considered leak free if it remained inflated. A one hour integrated sample was obtained at a rate 0.5 liters per minute for each run.

All sampling was conducted simultaneously.

4.5 Sample Recovery

A post test leak check of the particulate/SO₂ sampling train was performed at the completion of each run by sealing the nozzle and applying a vacuum equal to or greater than the maximum valve reached during the sample period. A leak rate of less than 0.02 CFM or 4 percent of the average sampling rate (whichever was less) was considered acceptable. The probe was then disconnected, the ice bath was drained and the remaining part of the sampling train was purged by drawing charcoal filtered air through the system for fifteen minutes at the average flow rate used during sampling. The nozzle and probe were then brushed and rinsed with reagent grade acetone and the washings were placed in clean polyethylene containers and sealed. The glass fiber filter was removed from the holder with forceps and placed in a covered Petri dish for return to the laboratory. The front half of the filter holder was rinsed with acetone and the washings were added to the nozzle and probe wash. The contents of impingers 1 through 3 were measured volumetrically and the silica gel in the fourth impinger was weighed to the nearest 0.1 gram for determination of moisture content. The 80 percent isopropanol in the first

impinger was discarded and the impinger was rinsed with demonized, distilled water. The 3 percent hydrogen peroxide in the second and third imingers was placed in a clean polyethylene sample bottle. The imingers, associated glassware and back half of the filter holder were then rinsed with de-ionized, distilled water which was added to the sample bottle.

Two calculations of the moisture content of the stack gas were made for each run, one from the impinger analysis and one from the assumption of saturated conditions based upon the average stack gas temperature and a psychrometric chart as described in EPA Method 4, Determination of Moisture Content in Stack Gases, 40 CFR 60, Appendix A. The lower of the two values of moisture content was considered to be correct and was used in the emissions computations.

5.0 ANALYTICAL PROCDURE

5.1 Pretest Preparation

The glass fiber filters for the particulate train were numbered, oven dried at 105°C for two to three hours, desiccated and weighed to a constant weight in preparation for the test. Results were recorded to the nearest 0.1 milligram. Filters were loaded into holders and a filter was set aside as a control blank. The imingers were charged as described in section 4.3 and the contents of the fourth impinger were weighed to the nearest 0.1 gram. The 3 percent hydrogen peroxide solution for the sulfur dioxide sampling was prepared the morning of the test from 30 percent reagent grade stock solution.

5.2 Analysis

Upon return to the laboratory, the particulate filters were removed from the containers with forceps, dried at 105°C for two to three hours, desiccated and weighed to a constant weight. Results were recorded to the nearest 0.1 milligram. The probe and nozzle washes and an acetone blank were measured volumetrically and transferred to clean, tared evaporating dishes and evaporated to dryness over low heat. The evaporating dishes were then oven dried at 105°C for two to three hours, desiccated and weighed to a constant weigh. Results were recorded to the nearest 0.1 milligram. The total particulate reported is the sum of the filter weight gain and the weight gain of the evaporating dishes, corrected for the acetone blank. The impinger solutions were analyzed for sulfur dioxide procedures specified in Section 4.3 of EPA Method 8.

PROJECT PARTICIPANTS AND CERTIFICATION

FIRST CALL CREMATORY B & L CREMATION SYSTEMS, INC. N20 SERIES HUMAN CREMATORY Clearwater, Florida

April 5, 2008

Project Participants:

Marke S. Gierke Byron E. Nelson Dale A. Wingler Travis B. Nelson

Kenneth M. Roberts

Certification:

I certify that to my knowledge all data submitted in this report is true and correct.

Byron E. Nelson, CIH

Southern Environmental Sciences, Inc.

1204 North Wheeler Street □ Plant City, Florida 33563 □ (813) 752-5014, Fax (813) 752-2475

VISIBLE EMISSION COMPANY FIRST Call Crimatory Não AA CrimaTory InciniryTore UNIT ADDRESS 12660 34 th ST. N # A-1 PERMIT NO. 1030473-003-AG YES NO 🗆 AIRS NO. EU NO. 1030473 PROCESS RATE PERMITTED RATE Advil SITE BALNZOAA CrimaTolz CONTROL EQUIPMENT AFTERBUINER OPERATING MODE AMBIENT TEMP. (* FI MIT. GES FIRE d STOP 4 HEIGHT ABOVE GROUND LEVEL START 130' STOP Jame HEIGHT RELATIVE TO OBSERVER START 230' STOP Jum DISTANCE FROM OBSERVER DIRECTION FROM OBSERVER START DO STOP START U90' STOP SUM STOP 50 EMISSION COLOR PLUMETYPE NIA NONE CONTIN. INTERMITTENT [] WATER-DROPLETS PRESENT? DETACHED IS IS WATER DROPLET PLUME YES 🗀 POINT IN PLUME AT WHICH OPACITY WAS DETERMINED START STOP SAME STOP same DESCRIBE BACKGROUND BACKGROUND COLOR STARTBINAT STOP SOME SKY CONDITIONS, START Scallered STOP Same WIND SPEED (MPH)
START 0-10 STOP DUME WIND DIRECTION START VOICE STOP VAC AVERAGE OPACITY FOR HIGHEST PERIOD RANGE OF OPACITY READINGS SOURCE LAYOUT SKETCH Comments

SEVALUATION									
OBSERV	ATION D	ATE	START	TIME 348		ı	STOP TIME		
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4_	(2		0	34	0	0	0	0
5	C	0	0	0	35	0	0	0	0
6	10	0	10	10	36	0	0	0	0
7	10	10	10	0	37	0	2	0	0
8	0	10	0	8	38	0	0	0	0
9	0	0	0	0	39	10	10	10	0
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13	2	13	0	0	43	0	0	10	0
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15	0	0	0	0	45	0	0	0	0
16	0	0		0	46	0	0	0	0
17 18	0	5	0	5	47	0	0	0	0
19	13	0	0	0	_48	0	$-\Box$	10	0
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Process Weight Statement

DATE 4 5 08	SAMPLING TIME: FROM 10.05A.M.	то <u>6 74</u> Р.М.					
STATEMENT OF DDOCESS WEIGHT							

COMPANY	FIRST Com Cagnarony.
MAILING ADDRESS SOURCE IDENTIFICATION	12660 3479 ST. N. CEGARLIATOR FL BEL Systoms N-20 SERIES CROMATSRY.
SOURCE LOCATION	12660 JUM ST. N. CLEARWATER PL

DATA ON OPERATING CYCLE TIME

END OF OPERATION,		
TIME		
ELAPSED TIME		
IDLE TIME DURING CYCLE		
DESIGN PROCESS RATING	PROCESS WEIGHT RATE (INPUT)	150 lb/Ar
	PRODUCT (OUTPUT)	,

DATA ON ACTUAL PROCESS RATE DURING OPERATION CYCLE

MATERIAL	Hunon	remaina	RATE	160 bs (Run)
MATERIAL		<u> </u>	RATE	155 lbs/ Run el
MATERIAL	- Ix		RATE	140 bs (24)
AVERAGE PROCESS WEIGHT		:	RATE	
PRODUCT			RATE	
PRODUCT		-	RATE	
PRODUCT			RATE	

I certify that the above information is true and correct to the best of my knowledge.

Name (Please Print)

Signature	
Title Openator.	

PARTICULATE MATTER COLLECTED

PARTICU	LATE MA	I LEK COLLU	CIDD		
PLANT: FIRST CALL CROM	ATTELY			- constancia	
UNIT NO.: B & L CREMATION SY	STEMS, I	NC. – N20 SE	RIES HUMAN	CREMATORY	
TEST DATE: 4/5/08		ANALYZE	ED BY:	<u> 16</u>	
Acetone blank container no.	405		Filter blank n	o. 6752	
	200		Filter blank to	are weight, g. 0.3402	
Acetone blank volume, ml., (VA)	101.0509			inal weight, g. 0.3409	
Acetone blank final weight, g. Acetone blank tare weight, g.	101.0507		Filter weight		
Acetone blank tare weight, g. Acetone blank weight diff., g. (ma)	0,00012		*		
Acetone plank weight until 8. (112)	0.000.2				
Run No.	t .	Container Number		articulate Collected	
		110111251	Final		Weight
			Weight	Tare Weight	Gain
Filter No.	6768	1 (Filter)	0.3603	0.3434	0.0169
Liquid lost during transport	0	2 (Wash)	103,1076	105.6522	0.0102
Acetone wash volume, ml (Vaw)	100		İ	Total	0.0271
Acetone wash reside, g.(Wa)	0.0001		!	Less acetone blank, g. (Wa)	0.0001
Acetone wash container no.	4 .	300.		Weight of particulate matter, g	0.0270
					
Run No.	2	- ""			
	2 6770	Container) At :- In the 6 TO	articulate Callacted	
Filter No.		Container Number		articulate Collected	Weight
Filter No. Liquid lost during transport, ml.	677 0	1	Final		Weight Gain
Filter No.	6770 · 0	Number		articulate Collected Tare Weight 0,3391	
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw)	6770 0 18	Number 1 (Filter)	Final Weight	Tare Weight	Gain
Filter No. Liquid lost during transport, ml. Acetone wash container no.	6770 0 18 125	Number	Final Weight 0.3972	Tare Weight 0,3391	Gain 0,0581
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw)	6770 0 18 125	Number 1 (Filter)	Final Weight 0.3972	Tare Weight 0,3391	Gain 0,0581 0,0111
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw)	6770 0 18 125	Number 1 (Filter)	Final Weight 0.3972	Tare Weight 0,3391 105,6522 Total	Gain 0.0581 0.0111 0.0692 0.0001
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw)	6770 0 18 125	Number 1 (Filter)	Final Weight 0.3972	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa)	Gain 0.0581 0.0111 0.0692
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw) Acetone wash reside, g.(Wa)	6770 0 18 125 0.0001	Number 1 (Filter)	Final Weight 0.3972	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate	Gain 0.0581 0.0111 0.0692 0.0001
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw)	6770 0 18 125	Number 1 (Filter)	Final Weight 0.3972	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate	Gain 0.0581 0.0111 0.0692 0.0001
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw) Acetone wash reside, g.(Wa)	6770 0 18 125 0.0001	Number 1 (Filter) 2 (Wash) Container	Final Weight 0.3972 105.6633	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate matter, g	Gain 0.0581 0.0111 0.0692 0.0001
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw) Acetone wash reside, g.(Wa) Run No.	6770 0 18 125 0.0001	Number 1 (Filter) 2 (Wash)	Final Weight 0.3972 105.6633	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate	Gain 0.0581 0.0111 0.0692 0.0001 0.0691
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw) Acetone wash reside, g.(Wa) Run No. Filter No.	6770 0 18 125 0.0001 3 6769 0 53	Number 1 (Filter) 2 (Wash) Container	Final Weight 0.3972 105.6633	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate matter, g	Gain 0.0581 0.0111 0.0692 0.0001 0.0691 Weight Gain
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw) Acetone wash reside, g.(Wa) Run No. Filter No. Liquid lost during transport, ml.	6770 0 18 125 0.0001 3 6769 0 53	Number 1 (Filter) 2 (Wash) Container	Final Weight 0.3972 105.6633 Weight of F	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate matter, g	Gain 0.0581 0.0111 0.0692 0.0001 0.0691
Filter No. Liquid lost during transport, ml. Acetone wash container no. Acetone wash volume, ml (Vaw) Acetone wash reside, g.(Wa) Run No. Filter No. Liquid lost during transport, ml. Acetone wash container no.	6770 0 18 125 0.0001 3 6769 0 53	Number 1 (Filter) 2 (Wash) Container Number	Final Weight 0.3972 105.6633 Weight of F Final Weight	Tare Weight 0,3391 105,6522 Total Less acetone blank, g. (Wa) Weight of particulate matter, g Particulate Collected Tare Weight	Gain 0.0581 0.0111 0.0692 0.0001 0.0691 Weight Gain

0.0001

0.0992

Less acetone blank, g. (Wa)

Weight of particulate matter, g

MOISTURE COLLECTED

Plant	FIRST CON CROWN	way.					
Unit Date Run N	NZOAA (remoter 4/5/08	<u>.</u>					
	Inpinger Number	1	2	3	4	Weighed by:	
	Final Weight (g):	160:0	104.0	_0_	259.4	DU	
	Initial Weight (g):	to <u>o.0</u>	10010	0_	<u> 257.3</u>	DY	
	Difference (g):	60.0	40	0	6.1		
	Total Condensate (g):		:		70.		
Unit Date Run N	Cherminal 45 OV					· · · · · · · · · · · · · · · · · · ·	
	Impinger Number	1	2	3	4	Weighed by:	
	Final Weight (grams)	195.0	105.0	0_0_	.366·8	M	
	Initial Weight (grams)	100.0	0000	0	259.2	DU	
	Difference (grams)	95.0	5-0	0	7.6		
	Total Condensate (grams)				107.6		
Unit Date Run#	4508.						
	Impinger Number Final Weight Initial Weight (grams) Difference (grams) Total Condensate (grams)	•	1 14.0 14.0 14.0	2 110 · 0 10 · 0	0 0	4 Weighed by: 263:2 <u>DV</u> 254:3 <u>DV</u> 8:9 62:4	

FIELD DATA SHEET

	r	IEED DATA SHEET	
Company Fic	st Call Cren	ratory	Run No.
Source <u>N20AA</u>	Crenatory	_	Date 4/5/08
Operator(s) MC/TN	10w !	24 hr. tin	ne at start 1005
•	•	24 hr. tir	ne at end 1167
Dimensions Dia	-1	Filter No	o(s). <u>-C764</u>
LxW 0	18.5"	Baromet	ric Pressure ("Hg) 30.39
Static Press. ("H2O)	<u>-0.03</u>	Elev Diff. Mano. 1	To Barom. (Ft.)
Meter Box No.	<u>_</u>	Ambient Tempera	ture (F°)
Meter ΔH@	1,450	·	
Meter Correction Factor	0.994	Assumptions	
Pitot Tube Cp	, ક્ષપ	% Moisture <u>IO</u>	Sample Train Leak Check:
Nozzle ID		Stack Temp. 1000	Initial O. W5 CFM @ 15 "Hg
Nozzle Dia. (Inches)	0.600	Meter Temp. <u>60</u>	Final O. 007 CFM @ 15 "Hg
Probe Length/Liner	3 quartz	Md/Ms 1.04	Initial Pilot Tube (-) (+)
·		K Factor 36.	Final Pitot Tube (-) (+)
		A Committee of the Comm	

llected: - In	np. No. 1	,Imp. l	No. 2 & 3	,Imp. No 4	,Tc	tal Filter	Tare Wt.		
Sample Time	Meter Vol. Vm	Vel. Head ΔΡ ("H2O)	Original Diff. AH ("H2O)	Stack Temp., Ts (sF)	Meter Temp., Tm (•F)	Hot Box Temp (•F)	Exit Temp. (•F)	Pump Vacuum ("Hg)	Other
0	234,328	.03	1,10	787	GQ		G^3		
2,5	236.03	163	1,10	796	69		63		
5.0	23764	,035	1.30	810	70		62		<u> </u>
7.5	239.34	.03	1.10	796		245			<u></u>
10.0	240,96	,03	1.10	802	73	244			
12.5	242,56	,03	1.40	806	75	240	58		
15,0	244.32	.03	1,40	808	77	241	58		
17.5		,02	.94	785	79	239			
20.0	247.70	,02	,94	דרר	४०	239			1
	249,21	,015	,58	783	QO.	237			<u> </u>
		.02		791	g (235	55		<u> </u>
		,02	,94	790	82	238	54	2.0	<u> </u>
		.02	,વવ	405	82	243	53	2.5	
	1		X.94	832	8.4	249	53	2.0	
35.0		.025	1,15	840	85	242	53	2.5	
		,025	1,15	839	86	240	53	2.5	
40.0			1,15	843	8 Ç	239	52	2.5	
42.5	261,49		1.35	851	87	235	53	2.5	
45,0	203,14			899	88	234	53	3.0	
47.5				905	90	233	52	3.0	
50.0			1,35	912	90	233	52	3.0	
			1.35	918	ao	235	52	3.5	
	·		1.35	921	91	238	51	3.0	
					92	240	51	3.5	
				 					
	Sample Time () 2,5 5,0 7,5 10,0 12,5 16,0 17.5 20,0 21,5 25,0 27.6 30,0 31,5 35,0 40,0 (),5	Time O 234,348 2,5 236,03 S,0 237,64 7,5 239,34 10,0 246,96 12,5 246,14 20,0 247,70 22,5 240,14 20,0 247,70 22,5 240,21 25,0 250,51 27,5 250,51 27,5 256,54 37,5 256,54 37,5 258,17 40,0 259,83 42,5 261,49 45,0 263,14 47,5 264,89 50,0 266,63 51,5 264,89 50,0 266,63 51,5 264,89 50,0 266,63 51,5 264,90 55,0 270,05 57,5 271,87	Sample Time	Sample Meter Vol. Vel. Head Office AH (H2O) O 334.348 .03 1.10 2.5 336.03 1.63 1.10 S.0 237.64 .035 1.10 10.0 240.96 .03 1.10 12.5 242.56 .03 1.40 15.0 244.32 .03 1.40 17.5 246.14 .02 .94 20.0 247.70 .02 .94 20.0 247.70 .02 .94 27.5 250.51 .02 .94 27.5 250.51 .02 .94 30.0 25350 .02 .94 30.0 25350 .02 .94 31.5 256.54 .025 1.15 27.5 261.49 .025 1.15 40.0 259.83 .005 1.15 40.0 259.83 .005 1.15 47.5 264.89 .035 1.35 50.0 266.63 .03 1.35 51.5 264.89 .036 1.35 51.5 264.89 .036 1.35 51.5 264.89 .036 1.35 51.5 264.89 .036 1.35 51.5 264.89 .036 1.35	Sample Time Vm Vel. Head Office AF (H2O) (Sample Time	Sample Time	Sample Time Meter Vol. Vel. Head Diff. AH Temp., Ts Temp., Hot Box Temp. Hot Box Temp. Temp. Hot Box Temp. Temp.	Sample Meter Vol. Yel. Head Original Dift. AH (FT) Temp., Ts (FT) Temp. (FT) Tem

FIELD DATA SHEET

Company Firs	f Call Crc.	natory	Run No
Source N20AA	Crematory	- -	Date <u>4/5/03</u>
Operator(s) TW/MG/	DW 1	24 hr.	time at start 13'48
		24 hr.	time at end 14:52
Dimensions Dia 10		Filter	No(s). <u>6770</u>
LxW	18.5"	Baron	netric Pressure ("Hg) 30, 639
Static Press ("H2O)	03	Elev Diff. Man	o. To Barom. (Ft.)
Meter Box No.	001	Ambient Temp	erature (F°)
Meter ΔH@	1,450	•	
Meter Correction Factor	0,994	<u>Assumptions</u>	
Pitot Tube Cp	, 84	% Moisture 10	Sample Train Leak Check:
Nozzle ID		Stack Temp. 400	Initial <u>0.002</u> CFM @ <u>15</u> "Hg
Nozzle Dia (Inches)	0.600	Meter Temp. 90	Final 0.002 CFM @ 12 "Hg
Probe Length/Liner	3 Quarte	Md/Ms 1.04	Initial Pilot Tube (-) (+)
		K Factor 39.85	Final Pitot Tube (-) (+)

Moist. Co	ollected: - In	np. No. l	,Imp.	No. 2 & 3	,Imp. No 4	,To	otal Filter	Tare Wt.	·	
Point#	Sample Time	Meter Vol. Vm	Vel, Head ΔΡ ('H2O)	Original Diff. AH ("H2O)	Stack Temp., Ts (•F)	Meter Temp., Tm (•F)	Hot Bax Temp (•F)	Exit Temp, (•F)	Pump Vacuum ("Hg)	Other
1	字 <i>O</i>	276403	.04	1.55	980	72	235	62	600	
2	2.5	278.68	,04	1.55	982	72	236	G1 =	6.0	
3	5.0	280,53	,04	1.55	984	74	235	60	6.0	
4	71.5	282.37	,04	1,55	965	75	231	59	6.0	
5	10.0	284.17	,045	1.74	1000	78	234	57	7.0	
6	12.5	280.12	.045	1.74	1005	80	237	57	7.5	
7	15.0	288.12	,04	1.55	1001	82	243	56	7,0	
8	17.5	290.04	.045	1.74) COG	84	2493	55	7,5	
9	20,0	292.03	,045	(.784	1012	дG	249	55	8,0	
10	22.5	294,06	,045	1,74	1017	87	246	54	8,0	
11	25.0	296.08	,૦૫	1,65	1012	88	259	54	8,0	1
12	27.5	298.05	104	1.55	1022	89	250	54	8.0	,
13	30,0	300.00	,04	1,55	006	90	254	53	8.0	
14	32.5	301.97	.045	1,74	1020	91	254	54	8.5	
15	35.0	303.90	.045	1.74	1021	93	258	53	9.0	
16	37.5	306,03	.045	1,74	1025	94	258	53	9.0	
17	40.0	300.07	1045	1,74	1028	95	258	53	9,6	
18	42.5	310,13	,045	1,74	1030	96	256	52	9,0	
19	45.0	312.18	.045	1,74	1034	94	253	52	9.0	
20	47.5	31424	,045	1.74	1033	98	2515	53	9.5	
21	<i>C</i> φ, υ	316.31	,04	1.55	1033	99	253	52	9,0	
22	52.5	316.31	.045	1,74	1036	99	252	52	9.0	
23	55,0	320,34	.045	1.74	[035	99	250	5(9,0	·
24	57,5	322.40	.045	1, 74	1038	100	248	51	9,5	
	00.0	304.49	1							

FIELD DATA SHEET

				. 7
Company Tres	f Call Crc	matory	Run No.	7
Source NOOAA	Crematory	_	Date	<u>45/08</u>
Operator(s) MG/TN	/pw 1	_	24 hr. time at start	1722
Oposas (v)			24 hr. time at end	1824
Dimensions Dia	,		Filter No(s).	6769
Dilitoriate to 1-62	18.5		Barometric Pressure	("Ha) 30.39
LxW 🗆	1813		Batomente Liessare	(118)
Static Press. ("H2O)	03	Elev Dif	f. Mano. To Barom. ((Ft.)
Meter Box No.	001	Ambient	Temperature (F°)	85
Meter ΔH@	1.450			
Meter Correction Factor	0.999	Assumptions		
Pitot Tube Cp	. 49	% Moisture 10		Train Leak Check:
Nozzle ID		Stack Temp. 100	-	005 CFM @ 15 "Hg
Nozzle Dia. (Inches)	0,600	Meter Temp. 100	Final O. C	009 CFM @ 12 "Hg
Probe Length/Liner	3 quartz	Md/Ms 1.00	Initial Pil	ot Tube (-) (+)
•		K Factor 36.	85 Final Pito	ot Tube (-)(+)
		:	_	

Moist, Co	ollected: - In	p. No. 1	,Imp. ì	No. 2 & 3	Imp. No 4	,To	otal Filter	Tare Wt.		
Point #	Sample Time	Meter Vol.	Vel. Head ΔP ("H2O)	Original Diff. ΔH ("H2O)	Stack Temp., Ts (*F)	Meter Temp., Tm (•F)	Hot Box Temp (•F)	Exit Temp. (•F)	Pump Vacuum ("Hg)	Other
1	0	331.948	.035	1.28	-932	42	237	_Sq	C/15	
2	2.5	333109	.035	1.28	1005	83	238	56	· 4,0	
3	5.0	33574	. 035	1.28	999	84	235	56	40	
4	7,5	33740	,04	1,47	1019	85	3.30	54	3.5	
5	10.0	339,25	,035	1.28	1012	86	232	54	3.5	
6	12.5	341,00	1035	1,28	1081	87	235	53	3.5	
7	15.0	342,70	,03	1.10	1020	88	231	53	3,5	
8	17.5	344,35	,03	1.16	1024	89	233	53	3,5	
9	20,0	345,95	103	1,10	1036	90	234	53	.3.5	
10	22.5	347,56	,025	,42	1039	91	235	52	3,5	
11	25.0	349,07		1,10	1088	.91	235	53	3.5	
12	27.5	350.09	,03	1,10	1028	.92	235	52	5.5	
13	30,6	352.34		1.47	1008	91	234	52	4.5	
	32.5	354.13	104	1,47	1053	43	234	<i>5</i> 9	5.0	
14 15	35.0	355,99	,04	1.45	1057	94	236	51	5.0	
	37.5	357.81	,04	1.47	1052	96	239	52	5.0	l
16 17	40.0	359,68	.04	1,47	1062	96	241	52	5.5	
18	42.5	361.54	.04	1,47	1075	96	243	51	5.5	
	45.0	363.38	,04	1.47	1083	97	245	51	5,0	
19	47.5	365.21	.035	1.28	1078	98	247	51	5.0	
20	:50,0	360,99		1,26	1073	98	248	51	5.0	
21	52.5	308.77	1035	1.28	1072	98	249	50	5.0	
22	55.0	370,54	.035	1,28	1071	98	849	50	5,0	
23	 	372.13	035	1,38	1059	98	245	90	6.0	
24	57.5	مىرىدىدى بەرلىنىدىدىدىدىدىدى رىدى ب		100	1	J.	 ~ . ~ . ~ 		T	1
	60.0	373,780	J	L		L		<u> </u>		

SOUTHERN ENVIRONMENTAL SCIENCES, INC. GAS ANAYLSIS DATA FORM

TANTO TATABLE OF THE STATE OF T
Plant: Royal Call Chemotory
Unit N-25 AA CRANSTON Test No.: 1
Date: 4 S O Sampling Loc: Stack
Sampling Time (24 hr. clock) 10:05 - 11:05
Sampling Type: Continuous □ Integrated Bag KGrab □
Analytical Method Orset Ambient Temp.
Operator MG

		Reading)	actual CO	1000 minus	N2 (Net is	Reading)	actual O2	Reading minus	Actual CO	CO (Net is	Reading)	actual CO2	Reading minus	Actual 02	02 (Net is	CO2	GAS		RUN-→
												-	ノズ・ウ			マチ	Reading	Actual	
												7	2.0			くぞ	Net		
												5	デジ			マント	Reading	Actual	2
												1.00	ن د			۸ أ	Net		
												100 100 1001 127	<u> </u>	•		5,2	Net Reading Net Reading	Actual	3
				, ' ,								(3)	ì `			がや	Net		
																			Average NetVolume
TATOI	TOTAL	.28		,	j	28			······································		.32					.44			Multiplier
										-		· · · · · · · · · · · · · · · · · · ·						•	Molecular Weight of Stack Gas(Dry Basis (MD)

SOUTHERN ENVIRONMENTAL SCIENCES, INC. GAS ANAYLSIS DATA FORM

Operator N/6	Analytical Method (CXSC)	Sampling Type: Continuous o Integrated Bag & Grab o	Sampling Time (24 hr. clock) 13: 48 - 14; 48	Date: 4508	Unit: 2. 20 pa Cremetoral	Plant Furth Call Comobor	
•	Ambient Temp. KO	X Grab □	4:48,	Sampling Loc.: Salek	Test No.: 2		

Rea	-	actu	100	S S	Rea	actu	Rea	Act	6	Rea	actu	Rea	Act	02	CO2	GAS		R
	Reading)	actual CO	1000 minus	N2 (Net is	Reading)	actual O2	Reading minus	Actual CO	CO (Net is	Reading)	actual CO2	Reading minus	Actual O2	O2 (Net is)2	S		RUN→
											-	5			5.1	Reading	Actual	₽*
											3	3			Š	Net		
												ĵ			۱. نا ا	Reading	Actual	2
		•	,								0.21	;			S-1	Net		
		٠									150 111 120)			o,s	Reading	Actual	w
`											1,2,1)		·	50	Net.		
																		Average NetVolume
TOTAL	.28				.28		•			.32					.44			Multiplier
																		Molecular Weight of Stack Gas(Dry Basis (MD)

SOUTHERN ENVIRONMENTAL SCIENCES, INC. GAS ANAYLSIS DATA FORM

Ç	
Plant Purst Call Crownbynn,	<i>y</i>
Unit: N. Zo As Compleyed, Test No.:	W
	Sampling Loc.:
Sampling Time (24 hr. clock) 17; 22 18122	
Sampling Type: Continuous o Integrated Bag & Grab o	
Analytical Method CX-2-1 Ambient Temp.	tTemp. &S,
Operator N. C	

	Reading)	actual CO	1000 minus	N2 (Net is	Reading)	actual 02	Reading minus	Actual CO	CO (Net is	Reading)	Reading minus actual CO2	Actual 02	02 (Net is	C02	GAS		RUN→
						•				:	18.4			è À	Reading	Actual	
											12.8			ē. N	Net		
		:		ï	-						8:3			S.2 4.5 4.5 6.8	Reading	Actual	2
		;				-					12.5			5.4	Net		
											8.4 12.8 18.3 12.9 18.5 13.0			N.N	Net Reading Net Reading	Actual	ω
	2	•									13.0			<i>5</i> ,8	Net		
					,						,						Average NetVolume
TOTAL	.28				.28					.32				.44			Multiplier
																	Molecular Weight of Stack Gas(Dry Basis (MD)

SOUTHERN ENVIRONMENTAL SCIENCES, INC. NOZZLE CALIBRATION

DATE: 4/5/08	BY: M6

Nozzle ID	Run No.	D1 (in.)	D2 (in.)	D3 (in.)	ΔD (in.)	DAVG (in.)
overt Z	1-3	- 600	. 599	. 601	.002	-600
		ļ				
-		1				

Where:

D1 D2 D3 =

Nozzle diameter measured on a different

Diameter (inches).

Tolerance = 0.001 inches

 ΔD

Maximum difference in any two

Measurements (inches).

Tolerance = 0.004 inches

Davg.

= Average of D_1, D_2, D_3

SAMPLE POINT LOCATIONS

Company: Fiest Can Crematisky.
Source: N. ZO AA CAGASTERY
Date: 4/5/08
Stack/Duct Dimensions: \%.5
Port Length: Yes X No
Points corrected for port length?
· ·
200
,
Sketch of Stack/Duct

Point	,
No.	Distance from Duct Wall (inches)
1	7.5
2	8.2
ے	912
4	10,3
<u>4</u> 5	11.6
_6	13.6
7	18.9
8	20 19
9	22·Z 23·3
lo.	23.3
11	24.3
12	25.0
<u></u>	
-	
	
	
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SOUTHERN ENVIRONMENTAL SCIENCES, INC. Type S Pitot Tube Inspection Form

· · · · · · · · · · · · · · · · · · ·			
Pitot Tube ID No.	00.INC		
Inspection Date	4/1/2002		
Inspected By	M. Gierke		
Pitot Tube Assembly Level? Pitot Tube Openings Damaged?	Yes (explain please)	No No	

ANGLE	MEASUREMENT	LIMITS
01	10	<10°
a2	10	<10°
bl	10	<5°
B2	10	<5°
	1.0	
0	2°	
A	.290 inches	
$z = A \sin Y$.010 inches	<1/8 inch
$\mathbf{w} = \mathbf{A} \sin \theta$.021 inches	<1/32 inch
Pa	.145 inches	
Pb	.145 inches	
Dt	.190 inches	

COMMENTS

1	CALIBRATION	YES	(NO)	
	REQUIRED			